## IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for preparing a silicon compound bearing at least one fluoroalkyl group by hydrosilylation of a fluoroalefin in the presence of a Pt-containing hydrosilylation catalyst, which comprises the process comprising:

- initially charging and heating a hydrogenchlorosilane;
- then metering in the fluoroolefin and reacting the reaction mixture; and
- and subsequently isolating the hydrosilylation product, and wherein a hydrosilylation catalyst based on is a hexachloroplatinic acid or a Pt(0) complex is used.

Claim 2 (Currently Amended): The process as claimed in claim 1, wherein,

- (i) a-the hydrogenchlorosilane is initially charged, heated, the hydrosilylation catalyst dissolved in an inert solvent is added and the fluoroolefin is then metered in; or
- (ii) a-the hydrogenchlorosilane is initially charged, heated and a mixture of fluoroolefin, hydrosilylation catalyst and optionally solvent is metered in; or
- (iii) a mixture of <u>the hydrogenchlorosilane</u> and the hydrosilylation catalyst dissolved in a solvent are initially charged, heated, and the fluoroolefin is metered in.

Claim 3 (Currently Amended): The process as claimed in claim 1 or 2, wherein the initially charged hydrogen-chlorosilane or the initially charged hydrogenchlorosilane-containing mixture is heated to a temperature in the range from 85 to 120°C.

Claim 4 (Currently Amended): The process as claimed in claim 1 or 2, wherein hydrogenchlorosilane and fluoroolefin are used in a molar ratio of from 3:1 to 0.5:1.

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Claim 5 (Currently Amended): The process as claimed in at least one of claims 1 to 4-claim 1, wherein toluene or xylene is used as an inert solvent.

Claim 6 (Currently Amended): The process as claimed in at least one of claims 1 to 5-claim 1, wherein the catalyst is used in a molar ratio of PT to hydrogenchlorosilane of from 1:100 000 to 1:100.

Claim 7 (Currently Amended): The process as claimed in at least one of claims 1 to 6-claim 1, wherein at least one hydrogenchlorosilane of the formula (I)

$$H(4-a-b)SiR_aX_b$$
 (I),

where wherein the groups R are identical or different and R is a linear, branched or cyclic alkyl group having from 1 to 20 carbon atoms or an aryl group,

the X is CI, and

a = 0, 1, 2 or 3, and

b = 0, 1, 2 or 3, and

 $1 \le (a+b) \le 3$ , is used.

Claim 8 (Currently Amended): The process as claimed in any of claims 1 to 7 claim 1, wherein a fluoroolefin is of defined purity-is used.

Claim 9 (Currently Amended): The process as claimed in any of claims 1 to 8 claim 1, wherein a the fluoroolefin having has an iodine content of less than 150 ppm by weight is used.

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Claim 10 (Currently Amended): The process as claimed in any of claims 1 to 9 claim

1, wherein a the fluoroolefin having has a diene content of less than 100 ppm by weight is used.

Claim 11 (Currently Amended): The process as claimed in any of claims 1 to 10 claim 1, wherein a the fluoroolefin having has a water content of less than 100 ppm by weight is used.

Claim 12 (Currently Amended): The process as claimed in any of claims 1 to 11 claim 1, wherein at least one fluoro-olefin of the formula II

$$R^1Y_mCH=CH_2$$
 (II),

where wherein R<sup>1</sup> is a monofluorinated, oligofluorinated, or perfluorinated alkyl group having from 1 to 12 carbon atoms or a perfluorinated aryl group, Y is a -CH<sub>2</sub>-, -0-, -0-CH<sub>2</sub>-, -S- group, and m is 0 or 1, is used.

Claim 13 (Currently Amended): The process as claimed in any of claims 1 to 12 claim 1, wherein a-the fluoroolefin is selected from the group consisting of

3,3,3-trifluoro-1-propene,

3,3,4,4,5,5,6,6,7,7,8,8,8-tridecafluorooctene,

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,10-tridecafluorooccene,

1,1,2,2-tetrafluoroethyl allyl ether,

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,10-heptadecafluorodecene,

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,11,11,12,12,12-hencosafluorooctene, and

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,11,11,12,12,13,13, [[-]]14,14,14-

pentacosafluorooctene-is-used.

Claim 14 (Currently Amended): The process as claimed in any of claims 1 to 13 claim 1, wherein the fluoroolefin is added to the initially charged hydrogenchlorosilane as set forth in (i) or (ii) or (iii) at a pressure of from 1 to 15 bar abs.

Claim 15 (Currently Amended): The process as claimed in any of claims 1 to 14 claim 1, wherein the fluoroolefin is metered in at a rate of from 50 to 300 I/h, based on 1 t of chlorosilane.

Claim 16 (Currently Amended): The process as claimed in any of claims 1 to 15 claim 1, wherein the reaction is carried out at a temperature in the range from 85 to 120°C and a pressure of from 1.5 to 50 bar abs. for a period of from 4 to 20 hours.

Claim 17 (Currently Amended): The process as claimed in any of claims 1 to 16 claim 1, wherein the hydrosilylation product is isolated from the product mixture by distillation and is subsequently esterified with an alcohol, where wherein the alcohol is used in an excess of from 0.1 to 10% and the alcohol used is denatured with ≤1 % by weight of methyl ethyl ketone or petroleum ether.

Claim 18 (Currently Amended): The process as claimed in any of claims 1 to 78 claim 1 carried out performed batchwise in a stirred tank reactor.